

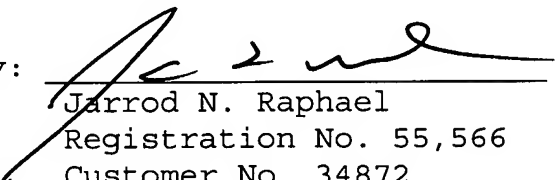
REMARKS:

Claims 1 - 12 are currently being amended to fix grammatical errors, and to conform to U.S. practice. Claims 3, 4, 6 - 10, and 12 are currently in multiple dependent formats in the above captioned pending application. The amendments to claims 3, 4, 6 - 10, and 12 are being made to directly remove the multiple dependencies found in each claim, and to conform to U.S. practice. These amendments do not introduce new matter within the meaning of 35 U.S.C. §132. Accordingly, entry of the amendments prior to examination is respectfully requested.

The Commissioner is hereby authorized to charge or deposit any deficiency or over payment to U.S. PTO Deposit Account 08-2336.

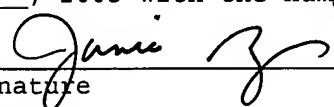
Respectfully submitted,

By:


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Date: September 29, 2005

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Signature

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ATTACHMENT A

1. (currently amended) A process for starting-up an olefin polymerization reaction in a gas-phase fluidized-bed reactor using a catalyst comprising a metallocene to produce a polyolefin having a melt flow rate of less than 4 g/10 min at 2.16 kg and a temperature of 190°C in accordance with ISO 1133 ~~of less than 4 g/10 min~~, wherein [[a]] said polyolefin having produced has an increased melt flow rate of above 4 g/10 min is produced during a transitional period during a start-up phase wherein said start-up phase has a duration of 30 minutes to 30 hours and said process is performed at a reaction temperature having a duration of from 30 minutes to 30 hours, in particular from 2 hours to 20 hours.

2. (currently amended) [[A]] The process as claimed in of claim 1, wherein the start-up phase has a duration of from 30 minutes to 30 hours, in particular from 2 hours to 20 hours.

3. (currently amended) [[A]] The process as claimed in either of the preceding claims of claim 1, wherein the melt flow rate of the polyolefin during the start-up phase is initially above 4.5 g/10 min and is continually decreased during the start-up phase to the melt flow rate of less than 4 g/10 min the value below 4 g/10 min.

4. (currently amended) The process as claimed in any of the preceding claims of claim 1, wherein the reaction temperature is increased prior to the start-up phase by at

least 1°C ~~compared in comparison~~ to the reaction temperature used in a long-term operation, ~~at least prior to the start-up phase.~~

5. (currently amended) [[A]] The process as claimed in of claim 4, wherein the reaction temperature is increased by from 1.5 to 4°C in comparison to the reaction temperature used in a long-term operation prior to the start-up phase.

6. (currently amended) [[A]] The process as claimed in claim 4 or 5, wherein the reaction temperature during the long-term operation of the reactor is in a range bounded by an upper limit given by equation I

$$T_{RH} = 170 + \frac{6d'}{0.84 - d'} \quad (I)$$

and a lower limit given by equation II

$$T_{RN} = 173 + \frac{7.3d'}{0.837 - d'} \quad (II)$$

~~where wherein, the variables have the following meanings:~~

T_{RH} is a maximum reaction temperature in °C

T_{RN} is a minimum reaction temperature in °C

d' is a value of the a density [[d]] of the polymer to be produced.

7. (currently amended) [[A]] The process as claimed in any of the preceding claims of claim 1, wherein the melt flow rate is regulated via the by hydrogen concentration in the reactor.

8. (currently amended) [[A]] The process as claimed in any of claims 1 to 6 of claim 1, wherein the melt flow rate is

regulated ~~via the~~ by a monomer partial pressure in the reactor.

9. (currently amended) ~~[[A]] The process as claimed in any of the preceding claims~~ of claim 1, wherein the polyolefin is a homopolymer or copolymer of ethylene.

10. (Cancelled).

11. (currently amended) ~~[[A]] The process as claimed in claim~~ ~~[[8]]~~ 1, wherein the metallocene is selected from bis(1-methyl-3-butylcyclopentadienyl)zirconium dichloride or bisindenylzirconium dichloride.

12. (currently amended) ~~[[A]] The process as claimed in any of the preceding claims~~ of claim 1, wherein an alkylaluminumoxane is used as an activating compound.